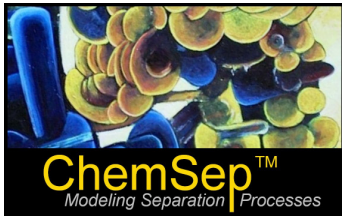
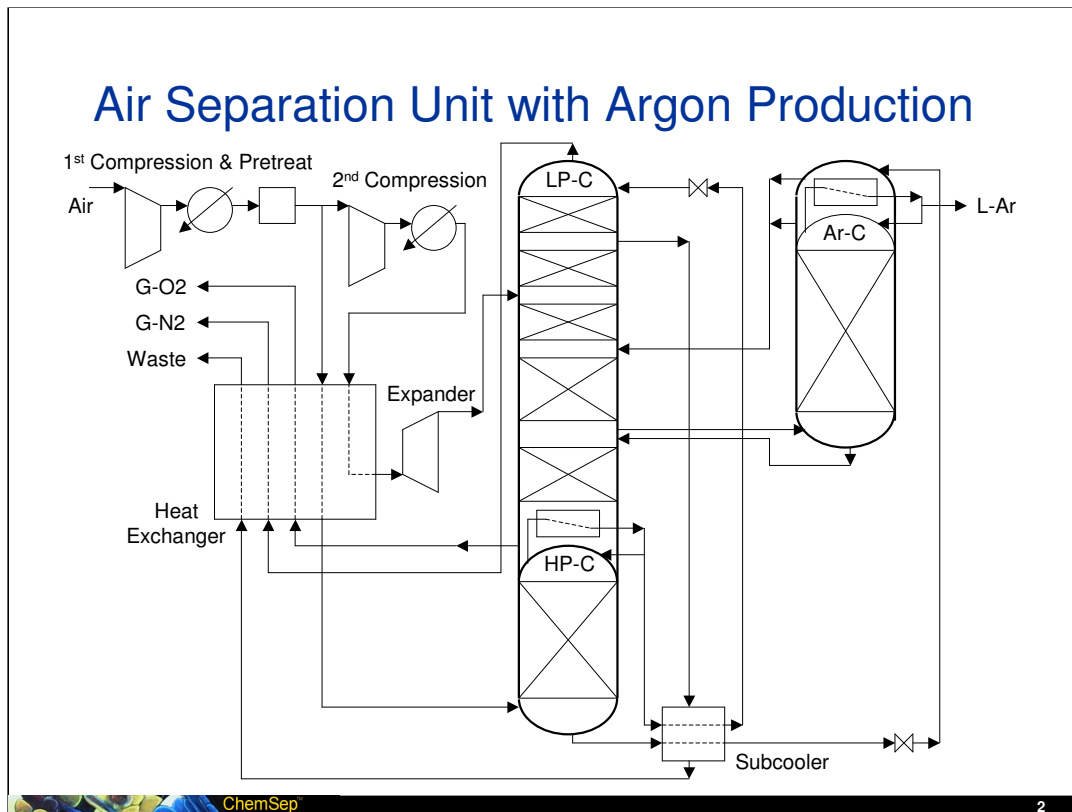


Simulation of an Air Separation Unit

ChemSep Case Book



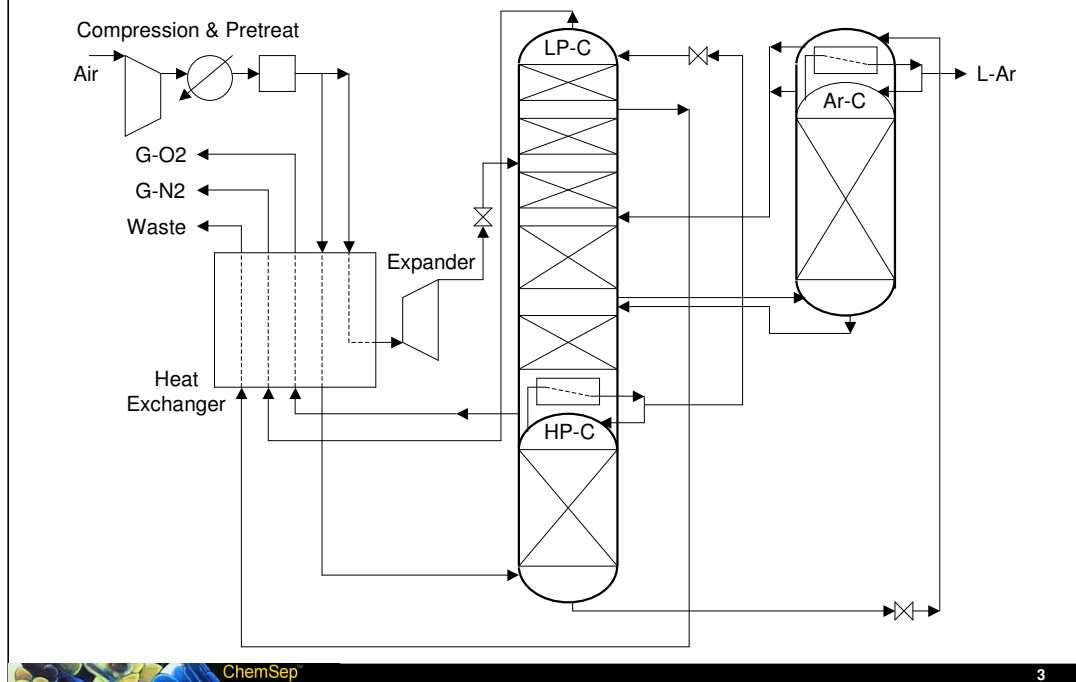
ChemSep Case Book <http://www.chemsep.com/downloads/index.html>
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The cryogenic air separation process is a tight integration of heat exchangers and separation columns which is completely driven by the compression of the air at the inlet of the unit. The air inlet stream is cooled and partially liquified against the leaving product streams. Nitrogen is then separated at a pressure of 6 bar in the first column and condensed against boiling oxygen at a lower pressure (around 1.2 bar). These two columns share the same column shell to minimize the temperature difference between the condensing nitrogen and evaporating oxygen. The liquid bottom product of the high pressure column is rich in oxygen and is reduced in pressure. The Joule-Thomson (JT) effect cools this rich liquid such that it can be used run the condenser of a side rectifier that separates Argon from Oxygen. This side rectifier is fed with a vapor side draw from the low pressure column. The whole process requires additional cooling which can be obtained using the JT effect in an expander, that feeds compressed air directly to the low pressure column. Thus, a certain part of the air cannot be separated but leaves the unit as a waste stream. Gaseous Nitrogen and Oxygen, and liquid Argon are the products. With temperature differences in the heat exchangers of just a few degrees Kelvin clearly there is significant interaction in these interconnected columns when any of the manipulated variables are adjusted or a disturbance affects one of the column controlled variables. Purities in Nitrogen and Argon are typically very high, with 1 ppm or less impurities. The oxygen product purity ranges from 97.5 to 99.5%.

See also *Comp.Chem.Eng.* Vol. 30 (2006) pp. 1436-1446.

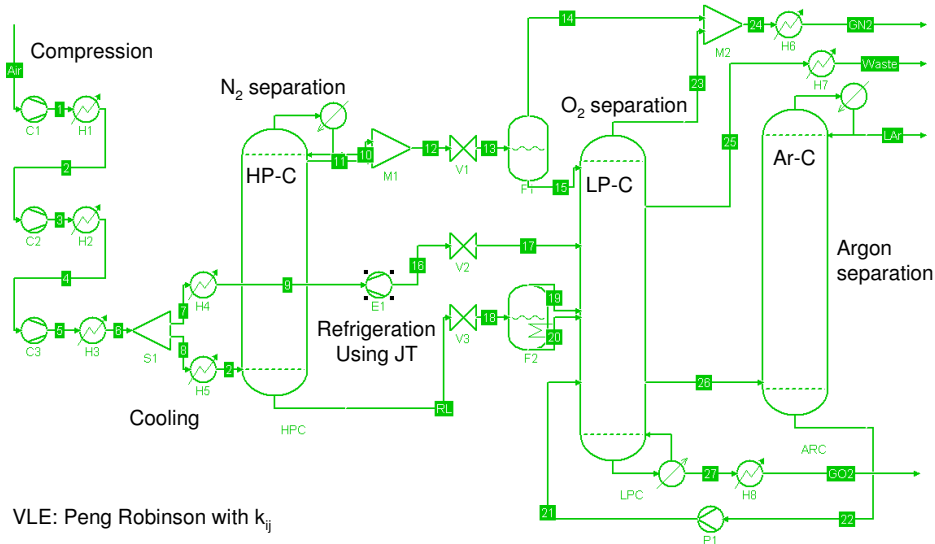
Simplified Simulation Air Separation Unit



In this simplified process of the Air Separation Unit (ASU) the 2nd compression stage and the subcooler are omitted at the expense of lower recoveries.

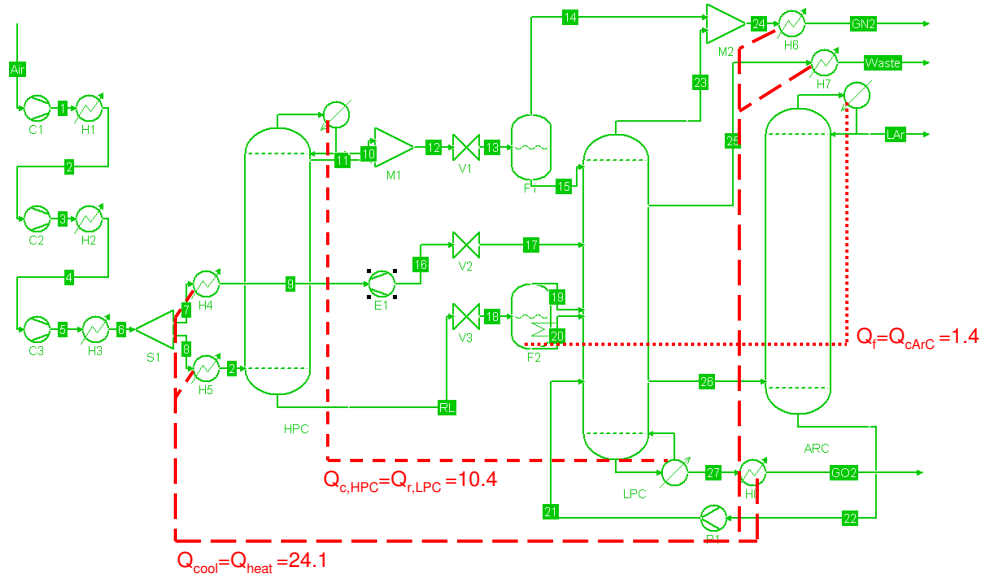
Air Separation Unit with Argon Production

With COCO: 5 iterations using stream estimate for stream 22



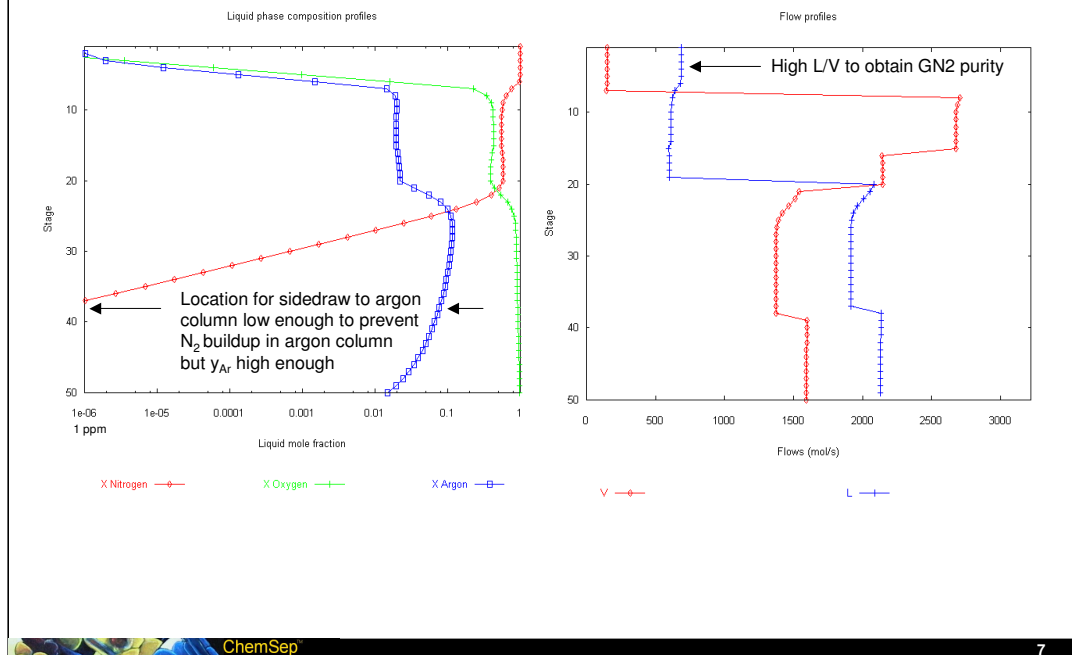
The process flowsheet as simulated in COCO of the simplified ASU. This flowsheet was simulated with one tear stream: the liquid stream 22 from the Argon column (Ar-C) back to the low pressure column (LP-C). Normally, the Argon column bottoms liquid flows back to the low pressure column by means of gravity. This is simulated by using a pump that raises the pressure of the bottoms liquid, as otherwise COCO warns us that the bottoms liquid would flow against a pressure gradient (the Argon column operates at a lower pressure than the low pressure column!). Also note that there is a vapor and a liquid drawn from the condenser of the high pressure column, for control purposes. This allows the high pressure column (HP-C) condenser and the low pressure column reboiler duties to be matched by a controller. The combined stream is fed to the top of the low pressure column (via a separator). The rich liquid bottom product of the high pressure column is flashed where the heat input is set equal to the condenser duty of the Argon side rectifier. The gaseous product streams are all heated up against the inlet air flow to recover heat.

Air Separation Unit: Heat Integration



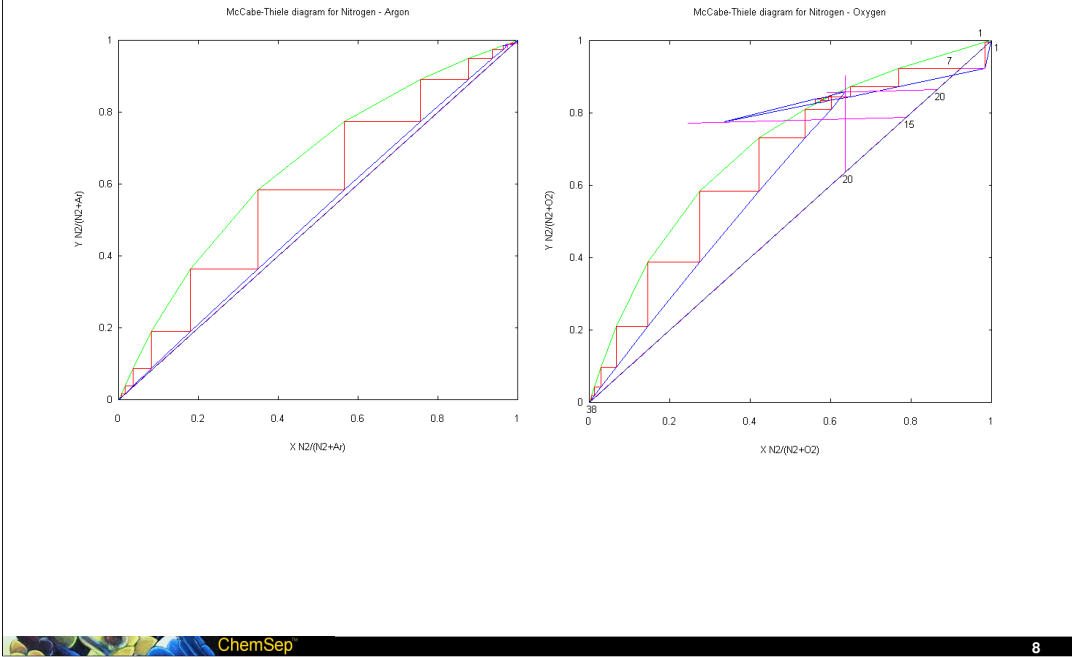
Here the three heat integrations in the ASU is shown: the cooling of the feed against the product streams in the main heat exchanger, the LP condenser against the HP reboiler, and the condensation of Argon against evaporation of rich liquid.

Air Separation Unit: Low Pressure Column



The internal flowrates in the LP-C must vary to obtain a pure gaseous Nitrogen top product as well as a reasonably pure oxygen in the bottoms. At the same time the vapor draw from the LP-C to the Ar-C must be low enough in Nitrogen to prevent buildup of N₂ in the Argon column, yet high enough in Argon for the Ar-C not to become pinched.

Air Separation Unit: Low Pressure Column



Easy McCabe-Thiele plots let the user quickly evaluate the process and the feed and draw locations to/from the low pressure column.

Binary Interaction Parameters

Peng-Robinson:

N_2/O_2 -0.0133

N_2/Ar -0.0026

O_2/Ar 0.0089

For a realistic simulation of the VLE in the ASU it is necessary to include the non-ideal behavior of the predominant three components in air. These interaction parameters for the Peng-Robinson EOS were obtained from DECHEMA.